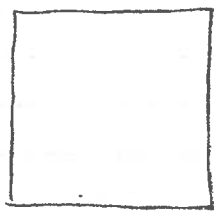


Homework #1 SOLUTIONS

1. Systems

6 points

a.



i. rigid tank, as described is closed

ii. ideal gas (one phase)

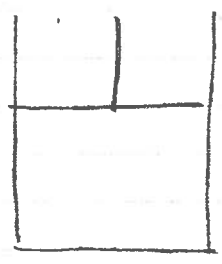
2 independent intensive properties

$T + P$ (okay in 1-phase)

$T + v$

$P + v$

b.



i. closed (no mass enters or leaves)

ii. $T + v$

$P + v$

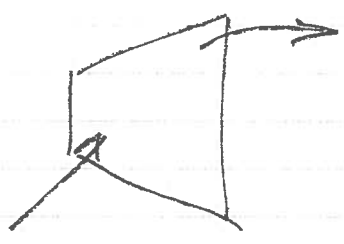
NOT $T + P$ for 2-phase

$T + x$

$P + x$

$v + x$

c.



i. open (steam enters and leaves turbine)

ii. heat $\{Q\}$
work $\{W\}$

2. Easiest to consider entire piston-cylinder (valve) and rigid tank as one closed system when

3 points

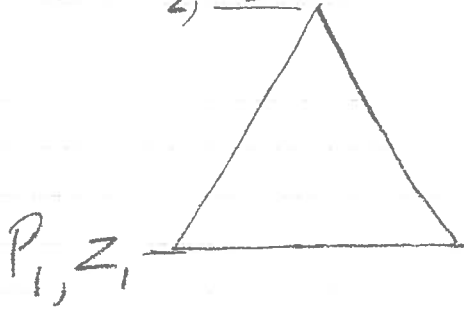
$$F + P_{atm}(A) = 200 \text{ kPa}(A) = 100 \text{ kPa}(0.03 \text{ m}^2) = 3 \text{ kN}$$

$$W = F \Delta x, \text{ where } \Delta x = \text{displacement} = -0.2 \text{ m (compression)}$$

2. b. $W = -0.2 \text{ m} (3 \text{ kN}) = \boxed{-0.6 \text{ kJ}}$
 (work done ON system)

c. $-W = \boxed{0.6 \text{ kJ}} = \text{work done by surroundings}$

3. P_2, z_2



$P_1 > P_2$ due to weight of column of air between z_2 and z_1 , for ρ_{air} and g constant

3. points

$$(P_2 - P_1)A = \rho g V$$

$A = \text{column area}$, $V = \text{column volume}$

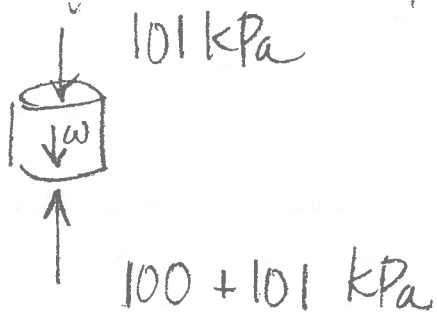
$$P_2 - P_1 = \rho g \frac{V}{A} = \rho g (z_2 - z_1)$$

check units: $\frac{\text{N}}{\text{m}^2} = \frac{\text{kg}}{\text{m}^3} \frac{\text{m}}{\text{s}^2} \text{m} = \frac{\text{N}}{\text{m}^2} \checkmark$

$$z_2 - z_1 = \frac{0.93 - 0.78 \text{ bars} (10^5 \text{ N/m}^2)}{(1.2 \text{ kg/m}^3) (9.81 \text{ m/s}^2) \text{ bar}}$$

$$z_2 - z_1 = \boxed{1.274 \text{ m}}$$

4. free body diagram on petcock



2 points

$$W_p + 101 \text{ kPa} (A_p) = 201 \text{ kPa} (A_p)$$

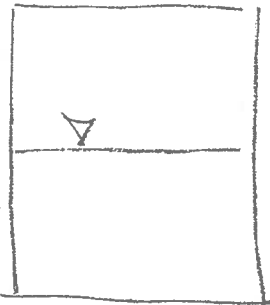
$$W_p = 100 \text{ kPa} (4 \text{ mm}^2) \left(\frac{10^{-6} \text{ m}^2}{\text{mm}^2} \right) \cdot 10^3 \frac{\text{N}}{\text{kN}}$$

$$= 0.4 \text{ N}$$

$$m_p = \frac{W_p}{g} = \frac{0.4 \text{ kg m/s}^2}{9.81 \text{ m/s}^2} = \boxed{0.041 \text{ kg}}$$

$$= 0.041 \text{ kg} \left(\frac{10^3 \text{ g}}{\text{kg}} \right) = \boxed{41 \text{ g}}$$

5.



$$V = 0.2 \text{ m}^3, \quad m = 1.5 \text{ kg}$$

liquid + vapor

$$V = m_g v_g + m_f v_f (= V_g + V_f)$$

where m_g = mass sat. vapor

m_f = mass sat. liquid

$$v_g = 0.1943 \text{ m}^3/\text{kg}$$

$$v_f = 1.127 \times 10^{-3} \text{ m}^3/\text{kg}$$

Also $m = m_g + m_f$

Substitute for $m_f = 1.5 - m_g$

$$0.2 \text{ m}^3 = 0.1943 m_g + (1.5 - m_g) 1.127 \times 10^{-3} \text{ (m}^3)$$

$$0.1983 \text{ m}^3 = (0.1943 - 1.127 \times 10^{-3}) m_g$$

5.

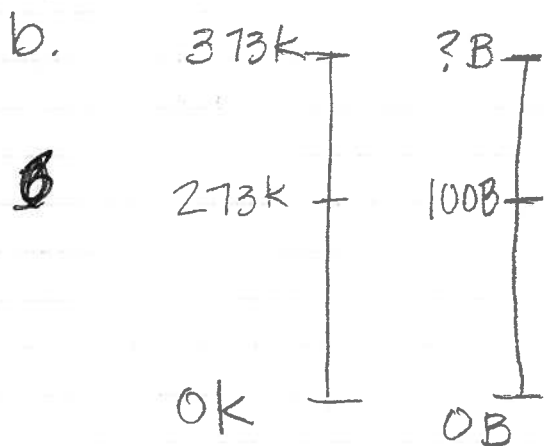
$$m_g = 1.027 \text{ kg}$$

$$m_f = 1.5 - 1.027 = 0.473 \text{ kg}$$

$$a. \quad V_g = m_g v_g = 1.03 \frac{\text{kg}}{\text{kg}} (0.1943) \text{ m}^3 = 0.1995 \text{ m}^3$$

$$b. \quad \frac{m_f}{m} = \frac{0.473 \text{ kg}}{1.5 \text{ kg}} = 0.315 \text{ OR } 31.5\%$$

6. a. 3 points Buff scale is valid absolute Temp scale if zero is lowest value and degrees are equal in size.



$$100 \text{ B} = 273 \text{ K}$$

$$1 \text{ B} = \frac{273}{100} \text{ K} = 2.73 \text{ K}$$

$$373 \text{ K} \left(\frac{1 \text{ B}}{2.73 \text{ K}} \right) = 137 \text{ B}$$

Boiling point of water (1 atm P) = 137 B

$$c. \quad ^\circ\text{C} = \text{K} - 273$$

$$20^\circ\text{C} = 293 \text{ K}$$

$$\frac{293 \text{ K}}{2.73 \left(\frac{\text{B}}{\text{K}} \right)} = \text{span style="border: 1px solid black; padding: 2px;">107 B \text{ (room temp)}$$