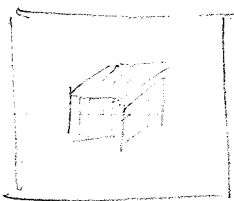


HW 10 SOLUTIONS

①

1.



$$0.01 \text{ kg chips } C_p = 0.3 \text{ kJ/kgK } T_0 = 20^\circ\text{C}$$

$$0.005 \text{ kg R-134a } T_1 = -40^\circ\text{C } x = 0$$

$$\Delta S_{\text{chip}} = S_2 - S_0 = m_c C_p \ln\left(\frac{T_2}{T_1}\right)$$

$$\Delta S_{\text{R-134a}} = S_2 - S_1 = m_R (S_2 - S_f), \quad S_1 = 0 \text{ (ref)}$$

Solution: system is adiabatic (assumed)

Assume $T_2 = -40^\circ\text{C}$ and test to see

if 1st & 2nd Law satisfied

1st Law: $Q = 0, W = 0$ for system

$$0 = m_c C (T_2 - T_0) + m_R (u_2 - u_1)$$

$$0 = 0.01 \text{ kg } 0.3 \frac{\text{kJ}}{\text{kgK}} (-40 - 20) = 0.005 \text{ kg } (u_2 - (-0.036)) \frac{\text{kJ}}{\text{kg}}$$

$$u_2 = 35.96 \text{ kJ/kg}$$

$$x_2 = \frac{35.96 - (-0.036)}{207.4} = 0.174$$

$$m_{g,R} = 0.174(0.005) \text{ kg} = 0.00087 \text{ kg}$$

so heat transfer ends when chips are @ -40°C

and 17.4% R-134a is vapor and $T_2 = -40^\circ\text{C}$

$$\Delta S_{\text{sys}} = \Delta S_c + \Delta S_R = 0.01 \text{ kg } 0.3 \frac{\text{kJ}}{\text{kgK}} \ln\left(\frac{233.1}{293}\right) - 0.005 \text{ kg } (S_2 - 0)$$

$$S_2 = 0.174(0.96856) + 0 = 0.16853$$

$$1. \Delta S_{sys} = 0.01(0.3) \left(\ln \left(\frac{233}{293} \right) \right) + 0.005(0.16853)$$

$$\Delta S_{sys} = -0.00069 + 0.00084$$

a) $\Delta S_c = \boxed{-0.00069 \frac{kJ}{K}}$

b) $\Delta S_R = \boxed{+0.00084 \frac{kJ}{K}}$

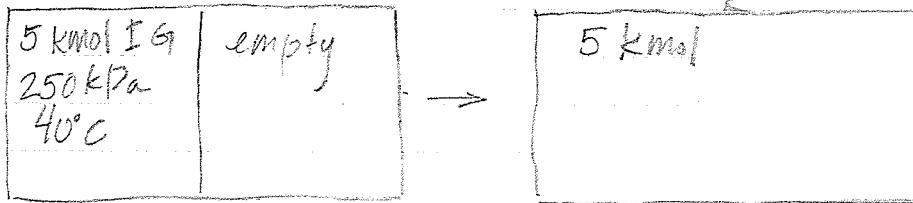
c) $\Delta S_{sys} = \boxed{0.00016 \frac{kJ}{K}}$

d) process is possible since

$$S_{gen} = \Delta S_{sys} - \frac{Q}{T} > 0$$

$$= 0.00016 \frac{kJ}{K} > 0$$

2.



adiabatic

a) $\Delta S = m \left[C_v \ln \left(\frac{T_2}{T_1} \right) + R \ln \left(\frac{v_2}{v_1} \right) \right]$

$$\frac{v_2}{v_1} = 2$$

process is adiabatic + passive

1st Law $0 = m C_v (T_2 - T_1)$

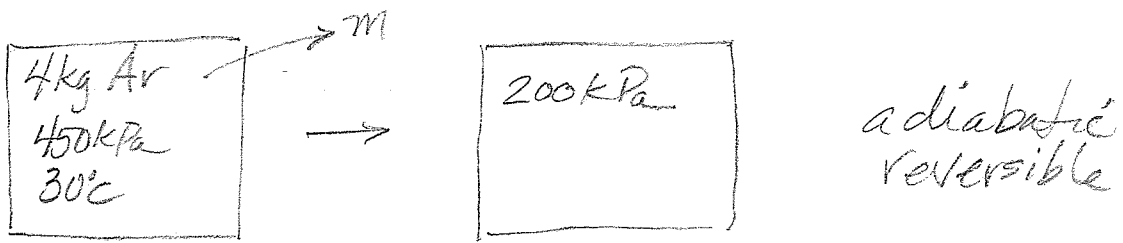
$T_2 = T_1 = 40^\circ C$ isothermal

$\Delta S = m R \ln \left(\frac{v_2}{v_1} \right)$ but $mR = N \bar{R}$

$\Delta S = N \bar{R} \ln \left(\frac{v_2}{v_1} \right) = 8.314 \frac{kJ}{kmol \cdot K} (5 \text{ kmol}) \ln(2)$

$\Delta S = \boxed{28.81 \frac{kJ}{K}}$

3.



$$s_2 - s_1 = 0 = m \left[C_p \ln\left(\frac{T_2}{T_1}\right) - R \ln\left(\frac{P_2}{P_1}\right) \right]$$

$$\ln\left(\frac{T_2}{303}\right) = \frac{0.2081 \ln\left(\frac{200}{450}\right)}{0.5203} = -0.3243$$

$$T_2 = 219K$$

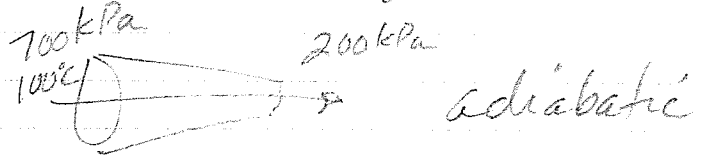
$$V = \frac{m_1 R T_1}{P_1} = \frac{4kg \left(\frac{0.2081 kJ}{kg \cdot K} \right) (303K)}{450 kPa}$$

$$V = 0.56 m^3$$

$$m_2 = \frac{P_2 V}{R T_2} = \frac{200 kPa (0.56 m^3)}{\frac{0.2081 kJ}{kg \cdot K} (219K)} = \boxed{2.46 kg}$$

4. $PV^{1.3} = C$

$$P_1 v_1^{1.3} = P_2 v_2^{1.3}$$



$$\left(\frac{v_1}{v_2}\right)^{1.3} = \frac{P_2}{P_1}$$

$$1.3 \ln\left(\frac{v_1}{v_2}\right) = \ln\left(\frac{P_2}{P_1}\right)$$

$$\frac{v_1}{v_2} = \exp\left(\frac{\ln(P_2/P_1)}{1.3}\right) = 0.381$$

$$\frac{P_1 v_1}{T_1} = \frac{P_2 v_2}{T_2}$$

a) $T_2 = T_1 \frac{P_2 v_2}{P_1 v_1} = 373K \left(\frac{200}{700}\right) \left(\frac{1}{0.381}\right) = \boxed{279.35K}$
 $= \boxed{6.35^\circ C}$

4. 1st law: $0 = c_p(T_2 - T_1) + \frac{V_2^2 - V_1^2}{2000}$

$$0 = 1.005(279.35 - 373) \frac{\text{kJ}}{\text{kg}} + \frac{V_2^2 - 900}{2000}$$

$$V_2 = 435 \text{ m/s}$$

ADD

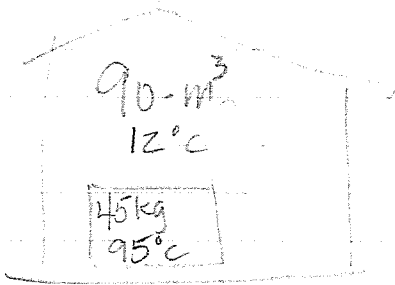
$$S_{gen} = c_p \ln\left(\frac{T_2}{T_1}\right) - R \ln\left(\frac{P_2}{P_1}\right)$$

$$= 1.005 \ln\left(\frac{279.35}{373}\right) - 0.287 \ln\left(\frac{200}{700}\right) - 0.2906 \frac{\text{kJ}}{\text{kgK}} \quad \left(- 0.360 \right)$$

$$S_{gen} = 0.069 \frac{\text{kJ}}{\text{kgK}}$$

possible
irreversible

5.



adiabatic

1st Law, $W = 0, Q = 0$

$$0 = m_w 4.184 \frac{\text{kJ}}{\text{kgK}} (T_2 - T_1) + \frac{P_1 V_1}{R T_1} (C_v (T_2 - T_1))$$

$$45 \text{ kg} (4.184 \frac{\text{kJ}}{\text{kgK}}) (95 - T_2) = \frac{101 (90)}{0.287 (285 \text{K})} (0.718 (T_2 - 12))$$

$$17,836.6 - 188.28 T_2 = 79.8 T_2 - 957.5 \text{ kJ}$$

$$T_2 = 70.3 \text{ } ^\circ\text{C}$$

$$b) \quad Q = m_w C (T_2 - T_1) = 45 (4.184) (70.3 - 95)$$

$$Q = -4652 \text{ kJ (from water to air)}$$

$$S_{gen} = m_w C \ln\left(\frac{343.3 \text{ K}}{368 \text{ K}}\right) + m_a C_v \ln\left(\frac{343.3 \text{ K}}{285 \text{ K}}\right) + R \ln\left(\frac{P_2}{P_1}\right)$$

$$= 45 (4.184) \ln\left(\frac{343.3}{368}\right) + 111.13 \text{ kg} (0.718) \ln\left(\frac{343.3}{285}\right)$$

$$5. \quad S_{gen} = -13.08 \frac{\text{kJ}}{\text{K}} + 14.85 \frac{\text{kJ}}{\text{K}} = \boxed{1.77 \frac{\text{kJ}}{\text{K}}} \quad (5)$$

(easier to note $v_2 = v_1$, since house is sealed, otherwise you would have to calculate $P_2 = P_1 \frac{T_2}{T_1}$ to solve for S_{gen} (same answer since $P_2 = 101 \left(\frac{3433}{285} \right) = 122 \text{ kPa}$)

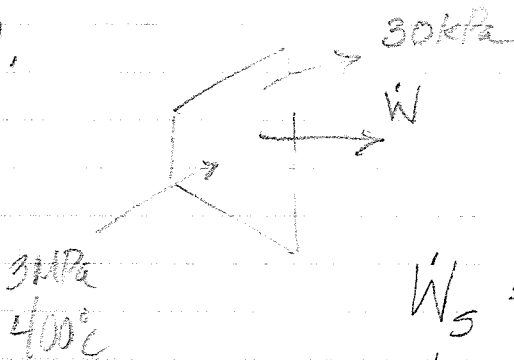
6. highest pressure = least work input = isentropic

(isothermal and adiabatic)
 $\dot{Q} = 0$
 $-\dot{W} = v(P_2 - P_1)\dot{m}$

$$P_2 = \frac{-(-25 \text{ kW})}{\frac{5 \text{ kg}}{3} (0.001 \text{ m}^3/\text{kg})} + 100 \text{ kPa}$$

$$P_{2 \text{ max}} = \boxed{5,100 \text{ kPa}}$$

7.



$$\dot{m}_{\text{steam}} = 2 \text{ kg/s}$$

$$\dot{W}_a = 0.92 \dot{W}_s$$

$$\dot{W}_s = \dot{m}(h_2 - h_1) \quad \text{for } s_2 = s_1$$

$$h_1 = 3231.7 \text{ kJ/kg}$$

$$s_1 = 6.9235 \text{ kJ/kgK}$$

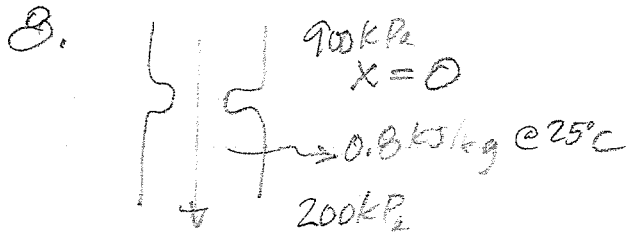
$$x_2 = \frac{6.9235 - 0.9441}{6.8234} = 0.876$$

$$h_2 = 0.876(2335.3) + 289.27 = 2335.7 \text{ kJ/kg}$$

$$\dot{W}_s = 2 \text{ kg/s} (3231.7 - 2335.7) = 1,792 \text{ kW}$$

$$7. \dot{W}_a = 0.92 (1792) \text{ kW} = \boxed{1649 \text{ kW}}$$

(6)



$$\text{1st Law } -0.8 \frac{\text{kJ}}{\text{kg}} = h_2 - h_1$$

$$h_1 = h_f @ 900 \text{ kPa} = 101.61 \text{ kJ/kg}$$

$$h_2 = q + h_1 = -0.8 + 101.61$$

$$h_2 = 100.81 \text{ kJ/kg}$$

$h_f < h_2 < h_g @ 200 \text{ kPa} \Rightarrow$ mixture

$$T = T_{\text{sat}} = -10.09 \text{ } ^\circ\text{C}$$

$$s_1 = s_f @ 900 \text{ kPa} = 0.37377 \frac{\text{kJ}}{\text{kg K}}$$

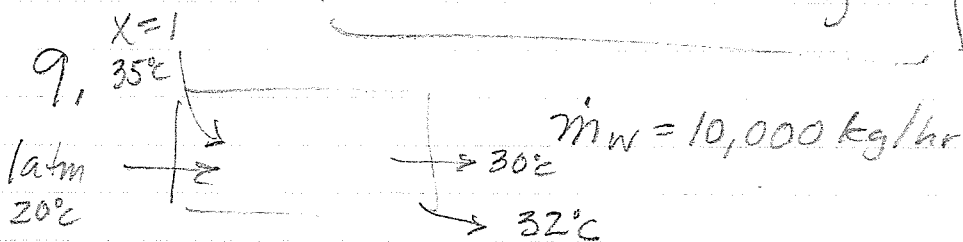
$$x_2 = \frac{100.81 - 38.43}{206.03} = 0.303$$

$$s_2 = 0.303(0.78316) + 0.15457 = 0.3919 \frac{\text{kJ}}{\text{kg K}}$$

$$s_{\text{gen}} = s_2 - s_1 - \frac{q}{T} = 0.3919 - 0.37377 - \left(\frac{-0.8}{298\text{K}} \right)$$

$$= 0.0181 + 0.00268$$

$$\boxed{s_{\text{gen}} = 0.0208 \frac{\text{kJ}}{\text{kg K}}}$$



9. $\dot{S}_{gen} = \dot{m}_w \Delta s_w + \dot{m}_a \Delta s_a$ since $\dot{Q} = 0$

\dot{m}_a from 1st Law $h_1 = h_3 @ 35^\circ C = 2564.6$

$0 = \dot{m}_w (h_2 - h_1)$

$h_2 \approx h_f @ 32^\circ C$

$\frac{32-30}{5} = \frac{h_2 - 125.74}{146.14 - 125.34}$

$h_2 = 134.3 \frac{kJ}{kg}$

$\dot{m}_a = \frac{\left(\frac{10000}{3600}\right) (2564.6 - 134.3)}{1.005 (10)} = 671.7 \frac{kg}{s}$

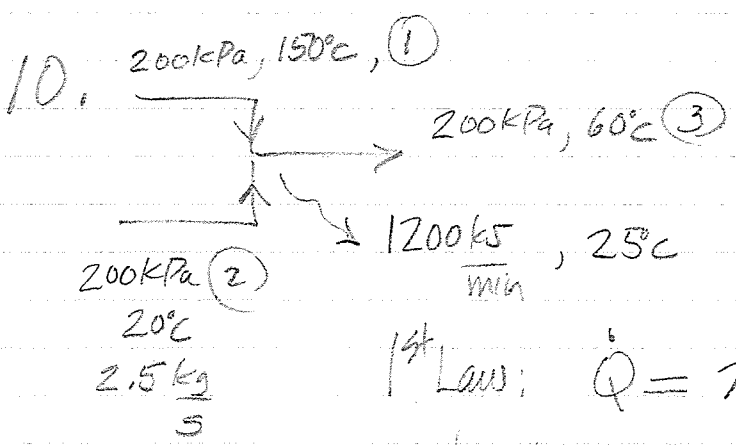
$\dot{m}_w \Delta s_w = \frac{10000}{3600} (s_2 - s_1)$ $s_1 = s_g @ 35^\circ C = 8.3517 \frac{kJ}{kg \cdot K}$
 $s_2 \approx s_f @ 32^\circ C$

$0.4 = \frac{s_2 - 0.4368}{0.5057 - 0.4368}$, $s_2 = 0.46412 \frac{kJ}{kg \cdot K}$

$= \frac{10000}{3600} (0.46412 - 8.3517) = -21.91 \frac{kW}{K}$

$\dot{m}_a \Delta s_a = 671.7 (1.005) \ln\left(\frac{303}{293}\right) = 22.66 \frac{kW}{K}$

$\dot{S}_{gen} = 22.66 - 21.91 = \boxed{0.745 \frac{kW}{K}}$



1st Law: $\dot{Q} = \dot{m}_3 h_3 - \dot{m}_2 h_2 - \dot{m}_1 h_1$

Continuity $\dot{m}_1 + \dot{m}_2 = \dot{m}_3$

$-20 \text{ kW} = (\dot{m}_1 + \dot{m}_2) h_3 - \dot{m}_1 h_1 - \dot{m}_2 h_2$

$-20 \text{ kW} = (\dot{m}_1 + 2.5) h_{f,60} - \dot{m}_1 (2769.1) - 2.5 (h_{f,20})$

10.

(8)

$$-20 \text{ kW} = (\dot{m}_1 + 2.5) 251.18 - \dot{m}_1 (2769.1) - 2.5 (83.915)$$

$$-438.16 = 251.18 \dot{m}_1 - 2769.1 \dot{m}_1$$

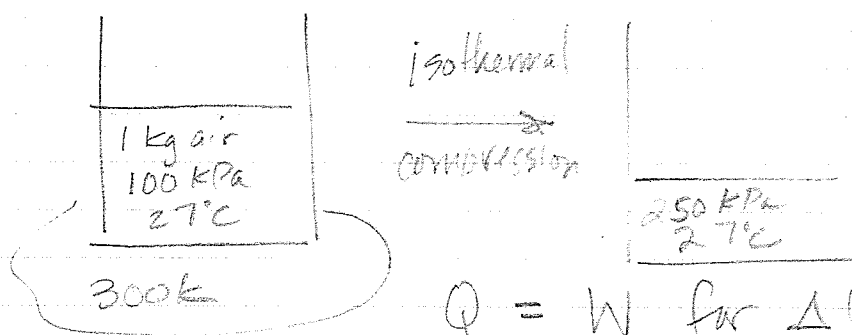
$$a) \quad \dot{m}_1 = \boxed{0.174 \text{ kg/s}}$$

$$b) \quad \dot{S}_{\text{gen}} = \dot{m}_3 s_{f,60} - \dot{m}_1 s_{1,150} - \dot{m}_2 s_{f,20} - \left(\frac{-20 \text{ kW}}{298 \text{ K}} \right)$$

$$\dot{S}_{\text{gen}} = (2.5 + 0.174) \text{ kg} \cdot 0.8313 \frac{\text{kJ}}{\text{kgK}} - 0.174 (7.281) - 2.5 (0.2965) + 0.0671$$

$$\dot{S}_{\text{gen}} = \boxed{0.282 \frac{\text{KW}}{\text{K}}} \quad \text{irreversible}$$

11.



$$P_1 V_1 = P_2 V_2$$

$$\frac{V_2}{V_1} = \frac{P_1}{P_2}$$

$$Q = W \text{ for } \Delta U = 0$$

$$Q = mRT_1 \ln\left(\frac{P_1}{P_2}\right) = 1 \text{ kg} \cdot 0.287 \frac{\text{kJ}}{\text{kgK}} \cdot 300 \text{ K} \ln\left(\frac{100}{250}\right)$$

$$Q = -78.8926 \text{ kJ}$$

$$\Delta S_{\text{air}} = -mR \ln\left(\frac{P_2}{P_1}\right) = (-1) \cdot 0.287 \ln\left(\frac{250}{100}\right)$$

$$\Delta S_{\text{air}} = -0.263 \frac{\text{kJ}}{\text{K}}$$

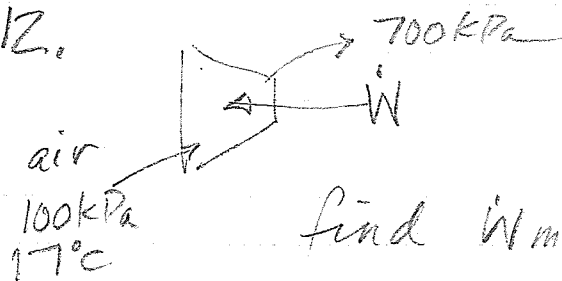
$$S_{\text{gen}} = -0.263 - \left(\frac{-78.8926}{300 \text{ K}} \right) = -0.263 + 0.263$$

$$\boxed{= 0}$$

satisfies 2nd Law

process must be reversible, which makes sense since $T_{\text{res}} = T_{\text{sys}}$ (no irreversibility)

12.



$$\dot{m} = 5 \text{ kg/min}$$

find \dot{W}_{\min} fora) adiabatic & reversible for min

$$\text{2nd Law: } s_2 - s_1 = 0 = \dot{m} \left[c_p \ln\left(\frac{T_2}{T_1}\right) - R \ln\left(\frac{P_2}{P_1}\right) \right]$$

$$\ln\left(\frac{T_2}{T_1}\right) = \frac{R}{c_p} \ln\left(\frac{P_2}{P_1}\right) = \frac{0.287}{1.005} \ln\left(\frac{700}{100}\right) = 0.556$$

$$T_2 = 290 \text{ K} (\exp 0.556) = 505.5 \text{ K}$$

$$\text{1st Law: } -\dot{W} = \dot{m} (h_2 - h_1) = \dot{m} c_p (T_2 - T_1)$$

$$= \frac{5}{60} \frac{\text{kg}}{\text{s}} (1.005 \frac{\text{kJ}}{\text{kgK}}) (505.5 - 290) \text{ K}$$

$$\boxed{-\dot{W}_{\min, \text{adia}} = 18.0 \text{ kW}}$$

b) isothermal reversible for min

$$\text{1st Law } \dot{Q} = \dot{W} \text{ since } \Delta T = 0$$

$$\text{2nd Law: } \dot{m} \Delta s_{\text{air}} = \frac{\dot{Q}}{T} + \dot{s}_{\text{gen}}^0$$

$$\dot{Q} = 290 \text{ K} \left(\frac{5 \text{ kg}}{60 \text{ s}} \right) \left[-R \ln\left(\frac{P_2}{P_1}\right) \right]$$

$$\dot{Q} = 290 \text{ K} \left(\frac{5 \text{ kg}}{60 \text{ s}} \right) \left[-0.287 \frac{\text{kJ}}{\text{kgK}} \ln\left(\frac{700}{100}\right) \right]$$

$$= -13.5 \text{ kW} = \dot{W}$$

$$\boxed{-\dot{W}_{\min, \text{isoth}} = 13.5 \text{ kW} < -\dot{W}_{\min, \text{adia}}}$$