

Homework 3 SOLUTIONS

①

1. state 1 (7 points - 1 each for a-g)

a) $v = 0.001 \frac{\text{m}^3}{\text{kg}}$ (A-4) $\frac{V_1}{v_1} = m = \frac{0.05 \text{ m}^3}{0.001 \frac{\text{m}^3}{\text{kg}}} = 50 \text{ kg}$

b) $v_2 = 0.79645 \frac{\text{m}^3}{\text{kg}}$ (A-5)

$V_2 = 50 \text{ kg} (0.79645 \frac{\text{m}^3}{\text{kg}}) = \boxed{39.8 \text{ m}^3}$

c) $h_1 \approx h_f @ 10^\circ\text{C} = 42.022 \text{ kJ/kg}$ (A-4)

$h_2 = 2967.9 \text{ kJ/kg}$ (A-6)

$\Delta H = m(h_2 - h_1) = 50 \text{ kg} (2967.9 - 42.022) \frac{\text{kJ}}{\text{kg}}$
 $= \boxed{146,294 \text{ kJ}} \times 10^{-3} \frac{\text{MJ}}{\text{kg}} = 146 \text{ MJ}$

d) $x_3 = 0.5$

$v_3 = 0.5(v_{fg}) + v_f @ 250^\circ\text{C}$

$= 0.5(0.050085 - 0.001252) + 0.001252 \frac{\text{m}^3}{\text{kg}}$ (A-4)

$v_3 = 0.02567 \frac{\text{m}^3}{\text{kg}}$

$V_3 = 50 \text{ kg} (0.02567 \frac{\text{m}^3}{\text{kg}}) = \boxed{1.28 \text{ m}^3}$

e) $P_3 = P_{\text{sat}} @ 250^\circ = \boxed{3976.2 \text{ kPa}}$
 $(\approx 4 \text{ MPa})$

f) $h_3 = 0.5(h_{fg}) + h_f @ 250^\circ\text{C} = 0.5(1715.3) + 1085.7 \frac{\text{kJ}}{\text{kg}}$
 $h_3 = 1943.4 \text{ kJ/kg}$

7 points

1. f) $\Delta H = m(h_3 - h_1) = 50 \text{ kg} (1943.4 - 42.022) \frac{\text{kJ}}{\text{kg}}$
 $\Delta H = 95,066 \text{ kJ}$ OR $\approx 95 \text{ MJ}$

(see graph)

2. (2 points)

Compressed liquid water @ 100°C, 15 MPa
find v, u, h from

$v \approx v_f @ 100^\circ\text{C} = 0.001043 \text{ m}^3/\text{kg}$

$u \approx u_f @ 100^\circ\text{C} = 419.06 \text{ kJ/kg}$

$h \approx h_f @ 100^\circ\text{C} = 419.07 \text{ kJ/kg}$

from Table A.7

$v = 0.0010361 \text{ m}^3/\text{kg}$ ($< 1\%$ difference)
 $u = 414.85 \text{ kJ/kg}$ (1% difference)
 $h = 430.39 \text{ kJ/kg}$ (3% difference)

3. (3 points)

Piston-cylinder with 0.8 kg steam @ 300°C and 1 MPa (superheated)

is cooled @ 300°C until $x = \text{~~0.25~~ } 0.25$ (1)

$T_2 = T_{\text{sat}} @ 1 \text{ MPa} = 179.9^\circ\text{C}$ (A.5)

$v_2 = (x v_{fg}) + v_f @ 1 \text{ MPa}$
 $= 0.25 (0.19436 - 0.001127) + 0.001127 \text{ m}^3/\text{kg}$
 $v_2 = 0.04944 \text{ m}^3/\text{kg}$

$V_2 = 0.8 \text{ kg} (0.04944 \text{ m}^3/\text{kg}) = 0.04 \text{ m}^3$

(see graph) $V_1 = 0.8 \text{ kg} (0.25799 \text{ m}^3/\text{kg}) = 0.2064 \text{ m}^3$
 $\frac{V_2}{V_1} = \frac{0.04}{0.2064} = 0.167$ (2)

4. Rigid tank with R-134a (isochoric process)
(3 points)

$$V = v m = 0.1450 (1 \text{ kg}) = 0.1450 \text{ m}^3$$

$$T_1 = -40^\circ\text{C} \quad v_f < v < v_g \text{ @ } -40^\circ\text{C}$$

① a) $P_1 = P_{\text{sat @ } -40^\circ\text{C}} = \boxed{51.25 \text{ kPa}}$
sat. mixture

① b) $P_2 = 200 \text{ kPa}$

$v > v_g \text{ @ } 200 \text{ kPa} \Rightarrow$ superheated R-134a

from A-13, $\boxed{T_2 = 90^\circ\text{C}}$

5. Ideal gas (O_2)
(2 points)

$$P_g = 500 \text{ kPa}, \quad V_1 = 1.3 \text{ m}^3$$

$$T_1 = 24^\circ\text{C}, \quad P_{\text{atm}} = 97 \text{ kPa}$$

Find m

$$PV = mRT \quad R = 0.2598 \frac{\text{kJ}}{\text{kg K}}$$

$$m = \frac{(500+97) \text{ kPa} (1.3) \text{ m}^3}{0.2598 \frac{\text{kJ}}{\text{kg K}} (273+24) \text{ K}} = \boxed{10 \text{ kg}}$$

(3 points) for $T = 25^\circ\text{C} = 298 \text{ K}$

$$P_g = 210 \text{ kPa}, \quad P_{\text{atm}} = 100 \text{ kPa}, \quad P = 310 \text{ kPa}$$

$$V = 0.025 \text{ m}^3$$

$$\frac{P_1}{T_1} = \frac{P_2}{T_2}$$

@ $T = 50^\circ\text{C} = 323 \text{ K}$ find $m_2 - m_1$, such that

$$P = 310 \text{ kPa}, \quad \text{assume } V_2 = V_1$$

6.
(3 points)

$$\textcircled{1} P_2 = T_2 (P_1 / T) = 323 \text{ K} \left(\frac{310 \text{ kPa}}{298 \text{ K}} \right) = 336 \text{ kPa}, \quad \Delta P = 26 \text{ kPa} \quad \textcircled{4}$$
$$P_1 V_1 = m_1 R T_1 \quad m_1 = \frac{310 (0.025) \text{ kJ-m}}{0.287 \frac{\text{kJ}}{\text{kgK}} (298 \text{ K})}$$
$$P_1 V_1 = m_2 R T_2 \quad = 0.0906 \text{ kg}$$

$$m_1 T_1 = m_2 T_2$$

$$\frac{m_2}{m_1} = \frac{T_1}{T_2}, \quad m_2 = 0.0906 \left(\frac{298}{323} \right)$$

$$m_2 = 0.084 \text{ kg}$$

$$m_1 - m_2 = 0.0906 - 0.084 = \boxed{0.007 \text{ kg}} \quad \textcircled{2}$$

7.
(2 points)

Ar, 0.2 kg, piston-cylinder, $V = 0.05 \text{ m}^3$

$P_1 = 400 \text{ kPa}$ isothermal expansion

$$V_2 = 2V_1 = 0.1 \text{ m}^3$$

find P_2 for ideal gas, isothermal expansion,
closed system,

$$P_1 V_1 = P_2 V_2$$

$$P_2 = P_1 \left(\frac{V_1}{V_2} \right) = 400 \text{ kPa} (0.5) = \boxed{200 \text{ kPa}}$$

8.
(2 points)

rigid tank, ideal gas @ 300 kPa, 600 K

$$m_2 = 0.5 m_1, \quad P_2 = 100 \text{ kPa}$$

1 a) find T_2 $P_1 V_1 = m_1 R T_1, \quad P_2 V_1 = m_2 R T_2$

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$$8.a) \quad \frac{m_1 T_1}{P_1} = \frac{m_2 T_2}{P_2} \quad m_1 = 2m_2$$

$$2 \frac{T_1}{P_1} = \frac{T_2}{P_2}$$

$$T_2 = 2 \left(\frac{P_2}{P_1} \right) T_1 = 2 \left(\frac{100}{300} \right) 600 \text{K}$$

$$T_2 = \boxed{400 \text{K}}$$

b) now $m_1 = m_2$

① $T_2 = 400 \text{K}$, find P_2

$$\frac{T_1}{P_1} = \frac{T_2}{P_2} \quad P_2 = \frac{T_2}{T_1} (P_1)$$

$$P_2 = 300 \text{kPa} \left(\frac{400}{600} \right) = \boxed{200 \text{kPa}}$$

9 (6 points) R-134a in piston-cylinder (not isobaric in process)

$m = 25 \text{kg}$, $P_1 = 320 \text{kPa}$, $v_1 = 0.0834 \text{m}^3/\text{kg}$

$v_1 > v_g @ 320 \text{kPa}$, superheated

① a) $T_1 = \boxed{70^\circ \text{C}}$ (A-13)

② b) $v_2 = v_1 = v_g \Rightarrow \boxed{\begin{matrix} P_2 = 240 \text{kPa} \\ T_2 = -5.38^\circ \text{C} \end{matrix}}$

9 c) isobaric condensation $T_3 = T_2 = \boxed{-5.38^\circ\text{C}}$

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① $V_3 = m v_3 = m v_f @ 240\text{kPa}$

$V_3 = 25\text{kg} (0.000762 \frac{\text{m}^3}{\text{kg}}) = \boxed{0.02 \text{ m}^3}$

① d)

$\Delta H = m(h_3 - h_1)$ $h_1 = 313.48 \frac{\text{kJ}}{\text{kg}}$
 $= 25\text{kg} (44.66 - 313.48) \frac{\text{kJ}}{\text{kg}}$ (A-13) $h_3 = h_f @ 240\text{kPa}$
 $= 44.66 \frac{\text{kJ}}{\text{kg}}$

$\Delta H = \boxed{-6,720 \text{ kJ}}$

① e)

Work = $\int_{v_1}^{v_3} P dv = \int_{v_2}^{v_3} P dv$

since $\int_{v_1}^{v_2} P dv = 0$ (constant v)

for $2 \rightarrow 3$, work @ $P = \text{constant}$ $W = P \int_{v_2}^{v_3} dv$
 $= P(v_3 - v_2)$ KN/m^2

$\bar{W} = P m (v_3 - v_2) = 240\text{kPa} (25\text{kg}) (0.000762 - 0.0834) \frac{\text{m}^3}{\text{kg}}$
Work = $\boxed{-496 \text{ kJ}}$ work done ON R-134a

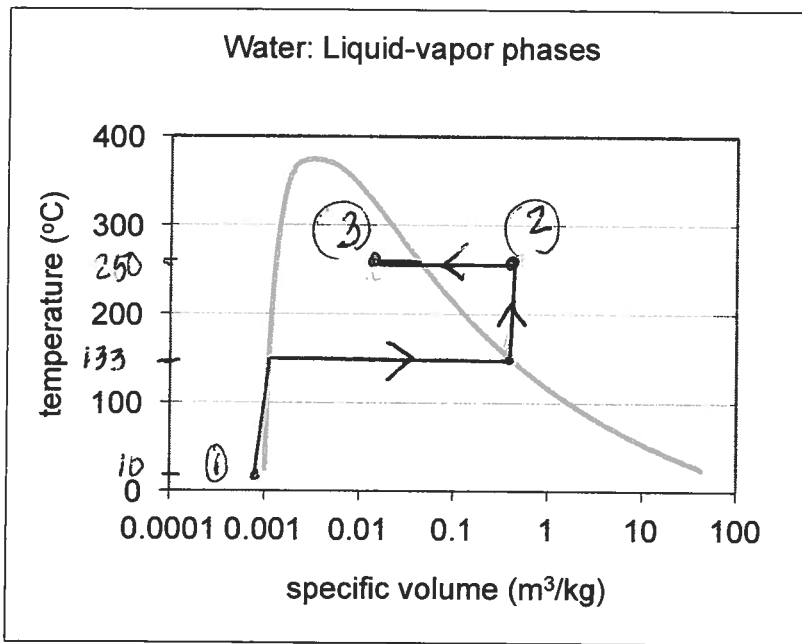
AREN 2110
Spring 2011

Homework #3: Due Friday, Feb. 4, 6 PM

- 3
1. A piston-cylinder device initially contains 50L of liquid water at 10 °C and 300 kPa. Heat is added to the water at constant pressure until the temperature reaches 250 °C. Determine the following:
 - a) the mass of the water
 - b) the volume after heating in m³
 - c) the enthalpy change after heating in kJ

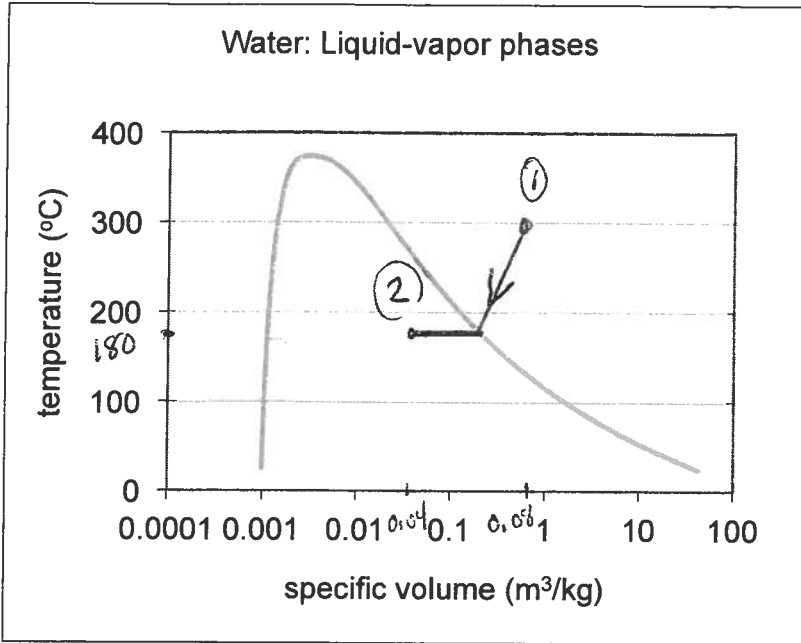
Now the water is compressed in an isothermal process until half the mass is in the liquid form.

- 4
- d) What is the final volume?
 - e) What is the final pressure?
 - f) What is the enthalpy change in the water for the 2-step process?
 - g) Show the two processes on the T-v diagram



CL
 $v \approx v_f @ T$
 $h \approx h_f @ T$
 $u \approx u_f @ T$

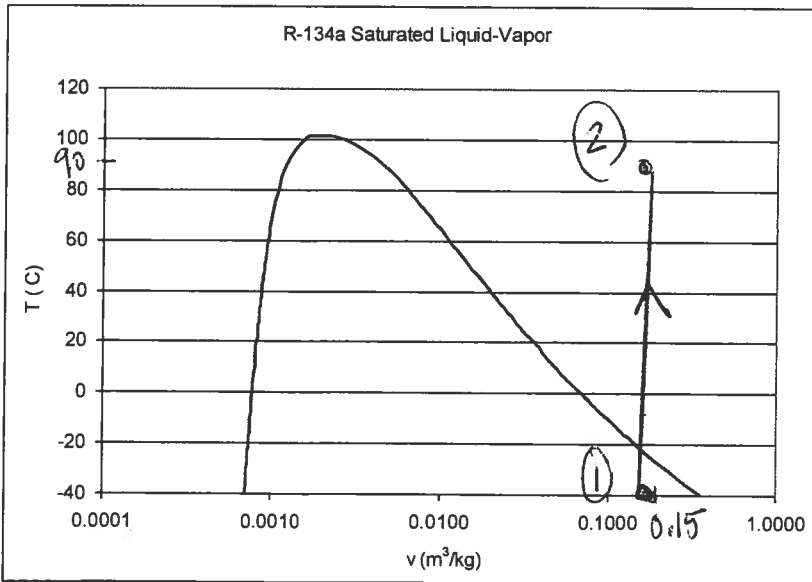
- 2
2. Determine the specific volume, internal energy and enthalpy of compressed liquid water at 100 °C and 15 MPa using the saturated liquid approximation. Compare these values to the ones obtained from the compressed liquid tables.
 - 3
 3. A piston-cylinder device contains 0.8 kg of steam at 300 C and 1 MPa. Steam is cooled at constant pressure until on 75% of its mass condenses. Show the process on a T-v diagram, find the final temperature and determine the volume change.



3

4. A rigid-wall tank with a volume of $0.1450 \text{ m}^3/\text{kg}$ contains one kg of R-134a at a temperature of $-40 \text{ }^\circ\text{C}$ (233K). The container is heated until the pressure of the R-134a is 200 kPa.

- / a) What is the initial pressure?
- / b) What is the final temperature of the R-134a?
- / c) Draw the process on the T-v diagram



2

5. The pressure gage on a 1.3 m^3 oxygen tank reads 500 kPa. Determine the amount of oxygen in the tank if the temperature is $24 \text{ }^\circ\text{C}$ and atmospheric pressure is 97 kPa.

calculate the work done between states 1 and 3. Is the work positive or negative?

f) Graph the process sequence on the P-V diagram (below)

