

# Practice problem solutions for midterm 1

①

1. 1 → 2 compression ( $m = 0.25 \text{ kg air}$ )

$$P_1 = 200 \text{ kPa}, P_2 = 300 \text{ kPa}, V_1 = 0.25 \text{ m}^3, V_2 = 0.1 \text{ m}^3$$

2 → 3  $V_3 = V_2 = 0.1 \text{ m}^3, P_3 = 100 \text{ kPa}$  (isochoric)

3 → 1  $P_3 = P_1 = 200 \text{ kPa}, V_3 = V_1 = 0.25 \text{ m}^3$

a) see graph

$$b) T_1 = \frac{P_1 V_1}{mR} = \frac{200 \text{ kPa} (0.25 \text{ m}^3)}{0.25 \text{ kg} (0.287 \frac{\text{kJ}}{\text{kgK}})} = 697 \text{ K} = 424^\circ \text{C}$$

c) without using  $K$  or  $A_p$ , geometric solution

$$A_{12} = W_{12} = \left( \frac{P_1 + P_2}{2} \right) (V_2 - V_1) = \boxed{-37.5 \text{ kJ}}$$

$$d) A_{31} = W_{31} = \left( \frac{P_3 + P_1}{2} \right) (V_3 - V_1) = \frac{(100 + 200)}{2} (0.25 - 0.1) = \boxed{W_{31} = 22.5 \text{ kJ}}$$

$$e) W_{23} = 0,$$

$$W_{\text{net}} = W_{12} + W_{31} = -37.5 + 22.5 = \boxed{-15 \text{ kJ}}$$

$$f. W_{3,12} = (300 - 200) \left( -\frac{0.15}{2} \right) = \boxed{-7.5 \text{ kJ}}$$

$$W_{331} = (200 - 100) \left( \frac{0.15}{2} \right) = \boxed{+7.5 \text{ kJ}}$$

same magnitude,  
opposite sign

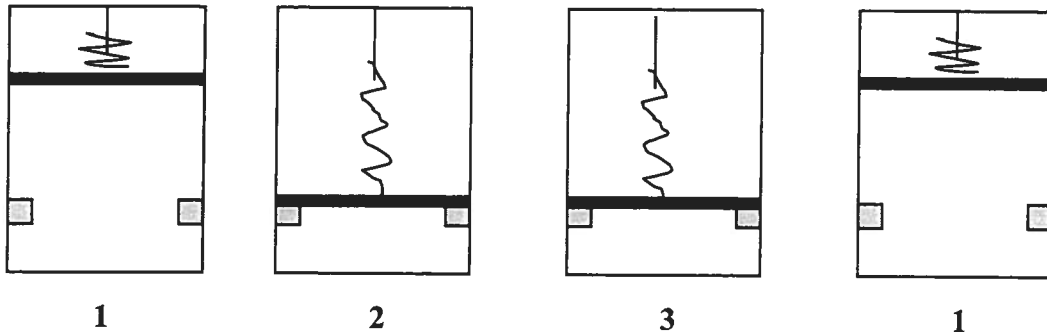
$$g) P_1 A + Kx = P_2 A$$

$$x = \frac{A(P_2 - P_1)}{K} = \frac{0.75 \text{ m}^2 (300 - 200 \text{ kPa})}{375 \text{ kN/m}} = \boxed{0.2 \text{ m}}$$

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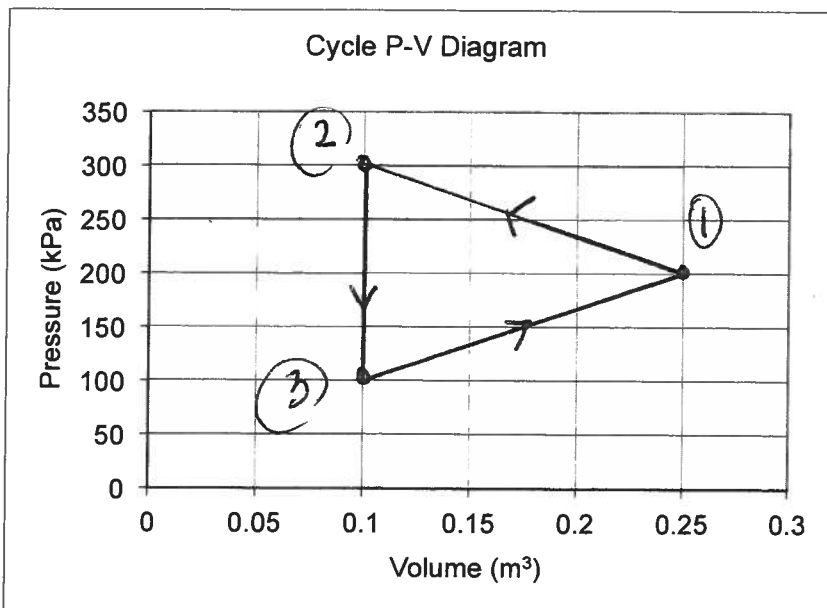
Practice Problems: State, Properties, and Work

1. A device consisting of a piston-cylinder with an attached spring containing 0.25 kg air is operated in the cycle described below



- 1 → 2: At state 1  $P_1 = 200 \text{ kPa}$  and  $V_1 = 0.25 \text{ m}^3$ . The compressed linear spring is released and the air is compressed until the spring no longer stores energy and the piston is just resting on the stops:  $P_2 = 300 \text{ kPa}$ ,  $V_2 = 0.10 \text{ m}^3$
- 2 → 3: After compression, heat is removed and the pressure drops to 100 kPa at state 3.
- 3 → 1: Then heat is added, the linear spring is compressed, and the air expands until it reaches state 1.

a) Draw the process on the P-V diagram below.



- b) Find the temperature of the air at states 1 and 3 ( $T_1$  and  $T_3$ ).
- c) Calculate the total work done during process 1  $\rightarrow$  2.
- d) Calculate the total work done during process 3  $\rightarrow$  1.
- e) Calculate the net work for the cycle, and note if work is being done by the system or on the system.
- f) Calculate the work done by the spring in process 1  $\rightarrow$  2. How does it compare with the work done on the spring in process 3  $\rightarrow$  1?
- g) If the spring constant = 375 kN/m and the area of the piston is 0.75 m<sup>2</sup>, what is the displacement of the spring for process 1  $\rightarrow$  2?

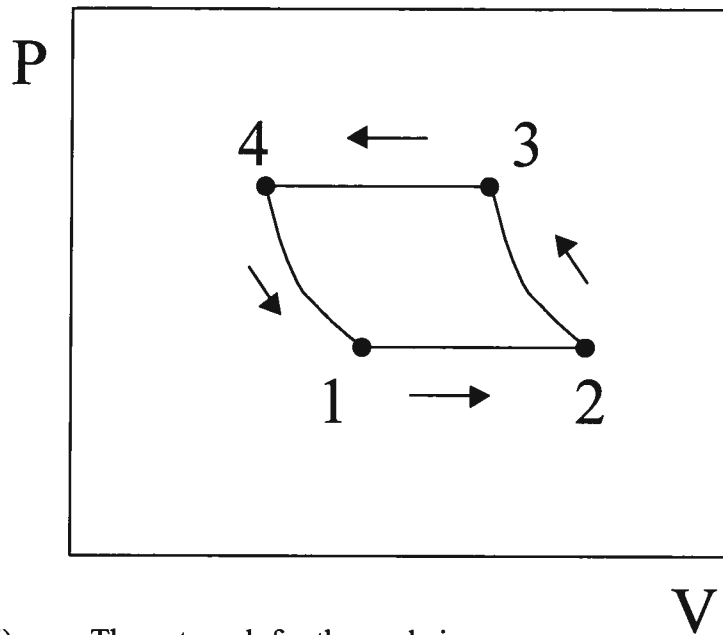
2. Complete the following table

	substance	P (kPa)	T (°C)	v (m <sup>3</sup> /kg)	x*	phase
①	H <sub>2</sub> O	200	120.21	0.3550	0.4	sat. liq-vapor mixture
②	H <sub>2</sub> O	200	85	0.001032	na	Compressed liquid
③	air	200	354	0.9	na	ideal gas
④	R-134a	200	-10.09	0.0500	0.50	sat liq-vapor mixture
⑤	R-134a	200	0	0.10481	na	superheated vapor

\* use "na" for "not applicable" where quality does not apply

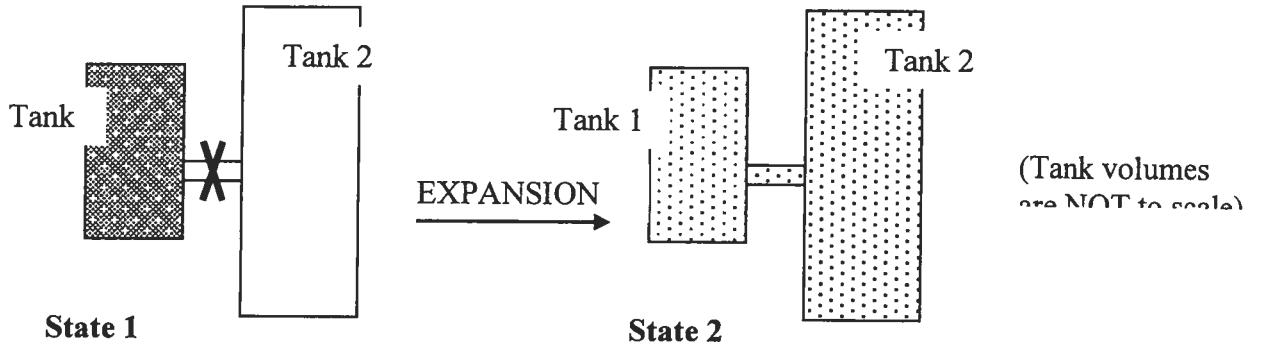
- ①  $v = x v_{fg} + v_f = 0.4(0.88578 - 0.001061) + 0.001061 = 0.3550 \text{ m}^3/\text{kg}$  (A-5)
- ②  $v \approx v_f @ 85^\circ\text{C}$  (A-4)  $T < T_{sat} @ 200 \text{ kPa}$
- ③  $T = Pv/R = 200 \text{ kPa} (0.9 \text{ m}^3/\text{kg}) / 0.287 \text{ kJ/kgK} = 627 \text{ K} = 354^\circ\text{C}$
- ④  $v_f < v < v_g @ 200 \text{ kPa}$  (A-12),  $x = (v - v_f) / v_{fg}$ ,  $T = T_{sat}$   
 $x = (0.05 - 0.0007533) / (0.099867 - 0.0007533) = 0.50$
- ⑤  $T > T_{sat} @ 200 \text{ kPa}$  (A-12) superheated  
 A-13  $v = 0.10481$

3. Use the P-V diagram below to answer the following questions



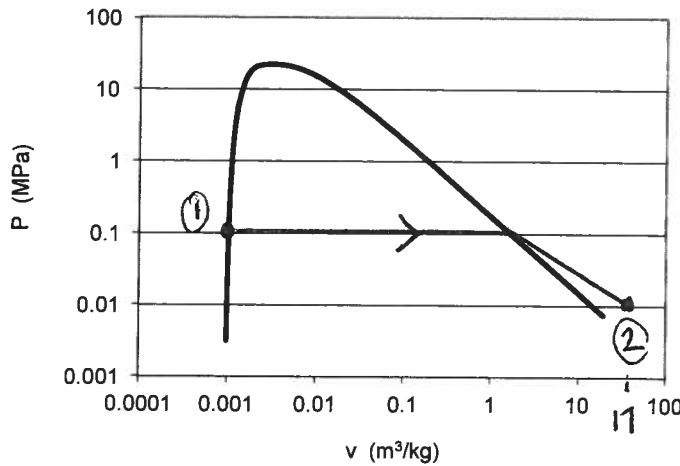
- i) The net work for the cycle is:
- a) Zero
  - b) Positive
  - c) Negative
  - d) Cannot tell from the diagram
- ii) The processes from states  $1 \rightarrow 2$  and  $3 \rightarrow 4$  are:
- a) Isothermal
  - b) Isobaric
  - c) Isochoric
  - d) Isometric
- iii) The net enthalpy change for the cycle is
- a) Zero
  - b) Positive
  - c) Negative
  - d) Cannot tell from the diagram

4. Ten (10) kg of saturated liquid water at 100 °C and 0.101 MPa with a specific volume of 0.001044 m<sup>3</sup>/kg is contained in a tank connected to an evacuated second tank through a pipe with a closed valve at state 1. The valve is opened and the water expands isothermally into the second tank until equilibrium is reached with 10 kg water at 100 °C and 0.01 MPa at state 2.



a) Draw the process on the P-v diagram below, showing process direction:

a) P-v diagram for water



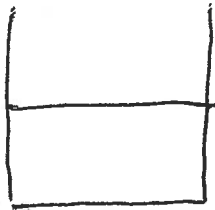
state 1:  
 sat. liquid water  
 @ 100°C, P = 0.101 MPa  
 state 2  
 T = 100°C, P<sub>2</sub> = 0.01 MPa  
 P<sub>2</sub> < P<sub>sat</sub> @ 100°C, superheated  
 v<sub>2</sub> = 17.196 m<sup>3</sup>/kg  
 (A-6)

b) Calculate the total volume of the two-tank system.

$$V_2 = m v_2 = 10 \text{ kg} \left( 17.196 \frac{\text{m}^3}{\text{kg}} \right) = \boxed{172 \text{ m}^3}$$

(6)

5.



$$H_2O, m = 1 \text{ kg}$$

$$V_1 = 0.2 \text{ m}^3$$

$$P_1 = 300 \text{ kPa}$$

$$v_1 = \frac{0.2 \text{ m}^3}{1 \text{ kg}} = 0.2 \frac{\text{m}^3}{\text{kg}}$$

a)  $v_f < v < v_g @ 300 \text{ kPa}$ , sat. mixture  $T = T_{\text{sat}} = \boxed{133.5^\circ \text{C}}$

b)  $v_2 = 0.6058 \text{ m}^3 = v_g @ 300 \text{ kPa}$  (isobaric expansion)

$$\text{heat required} = m(h_2 - h_1) = m(h_g - h_1)$$

$$h_1 = x h_{fg} + h_f @ 300 \text{ kPa}$$

$$x = \frac{v_2 - v_f}{v_{fg}} = \frac{0.2 - 0.001073}{0.60582 - 0.001073} = 0.329$$

$$h_1 = 0.329(2,163.5) + 561.43 = 1,273.1 \text{ kJ/kg}$$

$$h_g = 2724.9 \text{ kJ/kg}$$

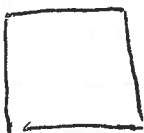
$$\text{heat required} = 1 \text{ kg} (2724.9 - 1273.1) = \boxed{1,452 \text{ kJ}}$$

c)  $T_{\text{sat}} @ 300 \text{ kPa} = \boxed{133.5^\circ \text{C}}$

d) A-6  $\boxed{T = 300^\circ \text{C}}$

e) see graph

6.



$$H_2O, m = 2 \text{ kg}, V = 0.2 \text{ m}^3, T = 200^\circ \text{C}$$

$$v = \frac{0.2}{2} = 0.1 \text{ m}^3/\text{kg} \quad v_f < v < v_g \text{ mixture}$$

a)  $P = P_{\text{sat}} = \boxed{1554.9 \text{ kPa}}$

b)  $x = \frac{0.1 - 0.001157}{(0.12721 - 0.001157)} = 0.784$

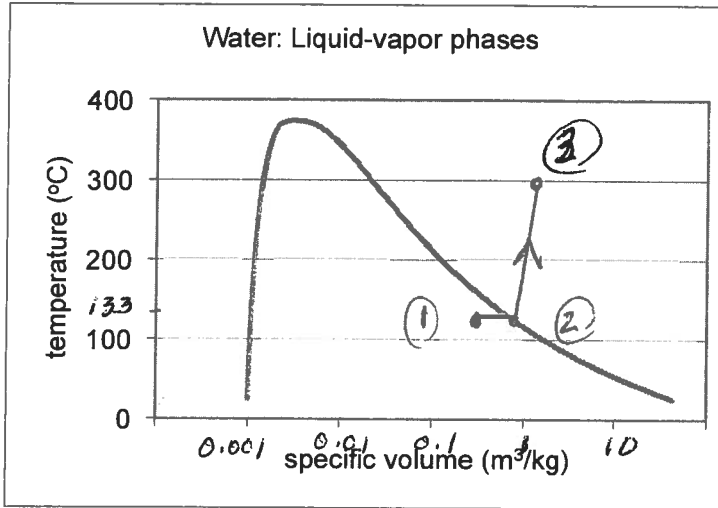
$$h = x h_{fg} + h_f = 0.784(1939.8) + 852.26 = \boxed{2373.3 \text{ kJ/kg}}$$

c)  $m_g = x m = 0.784(2) \text{ kg} = \boxed{1.57 \text{ kg}}$  vapor (sat)

d)  $V_g = m_g v_g = 1.57 \text{ kg} (0.12721 \text{ m}^3/\text{kg}) = \boxed{0.199 \text{ m}^3}$

5. One (1) kg of water in a piston cylinder device has an initial volume = 0.2 m<sup>3</sup>, and pressure of 300 kPa (constant throughout process).

- a) What is the water temperature?
- b) How much heat is required to expand the water to 0.6058 m<sup>3</sup>?
- c) What is the temperature after expansion?
- d) More heat is added until the volume = 0.8753 m<sup>3</sup>. What is the final temperature?
- e) Draw the process on a T-v diagram, showing values of for T and v.

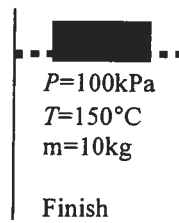
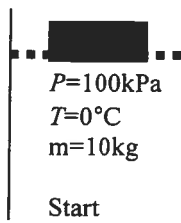


$v_1 = 0.2 \text{ m}^3/\text{kg}$   
 $v_2 = 0.6058 \text{ m}^3/\text{kg} \text{ (} v_g \text{)}$   
 $v_3 = 0.8753 \text{ m}^3/\text{kg}$   
 $T_1 = T_2 = 133.5^\circ\text{C}$   
 $T_3 = 300^\circ\text{C}$

6. The temperature of two kilograms of water contained in an 0.20-m<sup>3</sup> rigid tank is 200 °C. Determine:

- a) the pressure in the system
- b) the specific enthalpy of the system
- c) the mass of the vapor phase
- d) the volume of the vapor phase

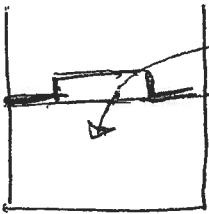
7. A piston/cylinder contains 10 kg of ice at  $T=0^\circ\text{C}$  and  $P=100\text{ kPa}$ . The ice is melted and then warmed to  $150^\circ\text{C}$  at constant pressure. (Latent heat of fusion of ice=333.7 kJ/kg @  $0^\circ\text{C}$ ).



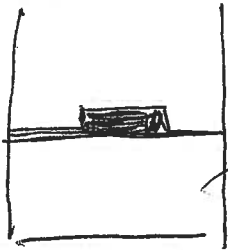
- a) How much energy is required to convert the ice to a saturated liquid?
- b) How much energy is required to convert the saturated liquid to the final state?
- c) What phase is the water at the end of the process?

8

7.



10 kg ice,  $T_i = 0^\circ\text{C}$ ,  $P = 100\text{ kPa}$   
 $h_i = 333.7\text{ kJ/kg}$  @  $0^\circ\text{C}$



10 kg,  $T = 150^\circ\text{C}$ ,  $P = 100\text{ kPa}$

a) energy required to melt ice and raise T from  $0^\circ\text{C}$  to  $T_{\text{sat}}$  @  $100\text{ kPa}$ ,  $x = 0$

$$\text{energy} = \Delta H = 10\text{ kg} (h_i + (h_f - h_i))$$

$$h_i \approx h_f @ 0^\circ\text{C} = "0" \text{ (ref for table A.4)}$$

$$h_f @ 100\text{ kPa} = 417.51\text{ kJ/kg}$$

$$\Delta H = 10 (333.7 + 417.51) = \boxed{7,512\text{ kJ}}$$

b) state 2  $P_2 = 100\text{ kPa}$ ,  $T_2 = 150^\circ\text{C} > T_{\text{sat}}$

superheated vapor at end

8.

convert Rankine to kelvin

$$491.7\text{ R} = 273\text{ K}$$

$$\boxed{1\text{ K} = 1.8\text{ R}} \text{ OR}$$

$$\text{BP } \text{H}_2\text{O} @ 1\text{ atm} = 273\text{ K} \left( \frac{1.8^\circ\text{R}}{\text{K}} \right) = \boxed{672\text{ R}}$$



9. He, isothermal compression  $T = 100^\circ\text{C}$

$$V_1 = 20\text{m}^3, V_2 = 2\text{m}^3, P_1 = 100\text{kPa}$$

(9)

$$a) m = \frac{P_1 V_1}{RT_1} = \frac{100\text{kPa}(20\text{m}^3)}{\frac{2.0769\text{kJ}}{\text{kgK}}(373\text{K})} = \boxed{2.58\text{kg}}$$

$$b) W_b = P_1 V_1 \ln\left(\frac{V_2}{V_1}\right) = 100\text{kPa}(20\text{m}^3) \ln\left(\frac{2}{20}\right) = \boxed{-4605\text{kJ}}$$

c) isobaric expansion  $V_3 = V_1 = 20\text{m}^3$

$$P_3 = P_2 = \frac{P_1 V_1}{V_2} = \frac{100\text{kPa}(20\text{m}^3)}{2\text{m}^3} = 1000\text{kPa}$$

$$T_3 = \frac{P_3 V_3}{mR} = \frac{1000\text{kPa}(20\text{m}^3)}{2.58\text{kg} \left(\frac{2.0769\text{kJ}}{\text{kgK}}\right)} = \boxed{3732\text{K}}$$

$$d) W_{\text{net}} = W_{b,12} + W_{b,23}$$

$$= -4605\text{kJ} + 1000\text{kPa}(20-2)\text{m}^3$$

$$W_{\text{net}} = \boxed{13,395\text{kJ}}$$

e) see graph

10.  $\text{H}_2$   $m = 3\text{kg}$   $R = 4.124\text{kJ/kgK}$

$$C_p = C_p @ 600\text{K} = 14.546\text{kJ/kgK}$$

$$\text{energy (Q)} = m C_p (T_2 - T_1) = 3\text{kg} \left(\frac{14.546\text{kJ}}{\text{kgK}}\right) 400\text{K}$$

$$= \boxed{17,455\text{kJ}}$$

$$P = \frac{mRT_1}{V_1} = \frac{3\text{kg} \left(\frac{4.124\text{kJ}}{\text{kgK}}\right) 400\text{K}}{10\text{m}^3} = \boxed{495\text{kPa}}$$

8. The Rankine scale is an absolute temperature scale. The ice point for water on the Rankine scale = 491.7 R.

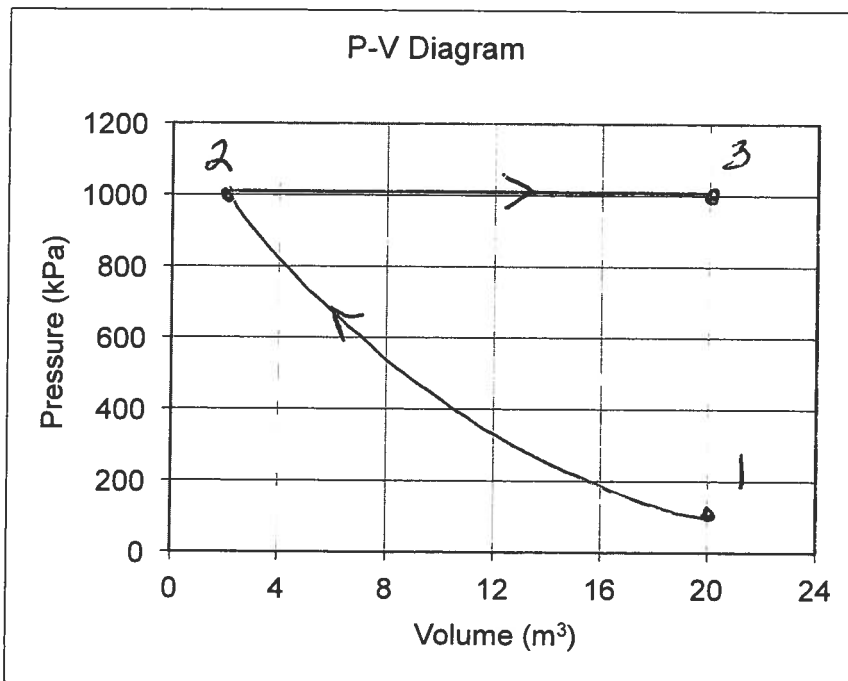
- a) Calculate the factor for converting from temperature in the Kelvin scale to the Rankine scale.
- b) What is the boiling point of water at 1 atm pressure in the Rankine scale?

9. Helium at 100 °C is compressed in a closed-system, isothermal process from an initial volume of 20 m<sup>3</sup> to a final volume of 2 m<sup>3</sup>. The initial pressure of the helium is 100 kPa.

- a) What is the mass of helium in the system?
- b) What is the boundary work done on the helium during the compression?

After compression, the helium is expanded at constant pressure to its initial volume.

- c) What is the final temperature of the helium?
- d) What is the net work of the entire two-step process?
- e) Draw the process on the P-V diagram below.



10. How much total energy is required to raise the temperature of 3 kg of hydrogen (H<sub>2</sub>), an ideal gas, from 400K to 800K in a constant pressure process where the volume of the gas increases from 10 m<sup>3</sup> to 20 m<sup>3</sup>? (Assume the temperature change is small enough that the specific heat is constant over the process.) At what pressure does this process take place?

(11)

11. Isobaric expansion R-134a

$$P = 0.1 \text{ MPa}, T_1 = -32^\circ\text{C}, V_1 = 0.1 \text{ m}^3$$

$$T_2 = 30^\circ\text{C}$$

$$a) \quad m = \frac{V_1}{v_1} \quad T_1 < T_{\text{sat}} @ 100 \text{ kPa}$$

$$m = \frac{0.1 \text{ m}^3}{0.0007172 \text{ m}^3/\text{kg}}$$

compressed liquid

$$v_1 \approx v_f @ -32^\circ\text{C} = 0.0007172 \text{ m}^3/\text{kg}$$

$$m = \boxed{139 \text{ kg}}$$

b)  $30^\circ\text{C} > T_{\text{sat}} @ 100 \text{ kPa}$  (superheated)

$$v_2 = 0.24233 \text{ m}^3/\text{kg}$$

$$V_2 = 139 \text{ kg} \left( 0.24233 \frac{\text{m}^3}{\text{kg}} \right) = \boxed{33.8 \text{ m}^3}$$

$$c) \quad h_1 = h_f @ -32^\circ\text{C} = 10.1 \text{ kJ/kg}$$

$$h_2 = 280.68 \text{ kJ/kg}$$

$$\Delta H = m(h_2 - h_1) = 139 \text{ kg} (280.68 - 10.1 \frac{\text{kJ}}{\text{kg}})$$

$$\Delta H = \boxed{37,610 \text{ kJ}}$$

d) isothermal compression, to sat liquid @  $30^\circ\text{C}$ 

$$P = P_{\text{sat}} @ 30^\circ\text{C} = \boxed{770.64 \text{ kPa}}$$

e) see graph

$$f) \quad h_3 = h_f @ 30^\circ\text{C} = 93.58 \text{ kJ/kg}$$

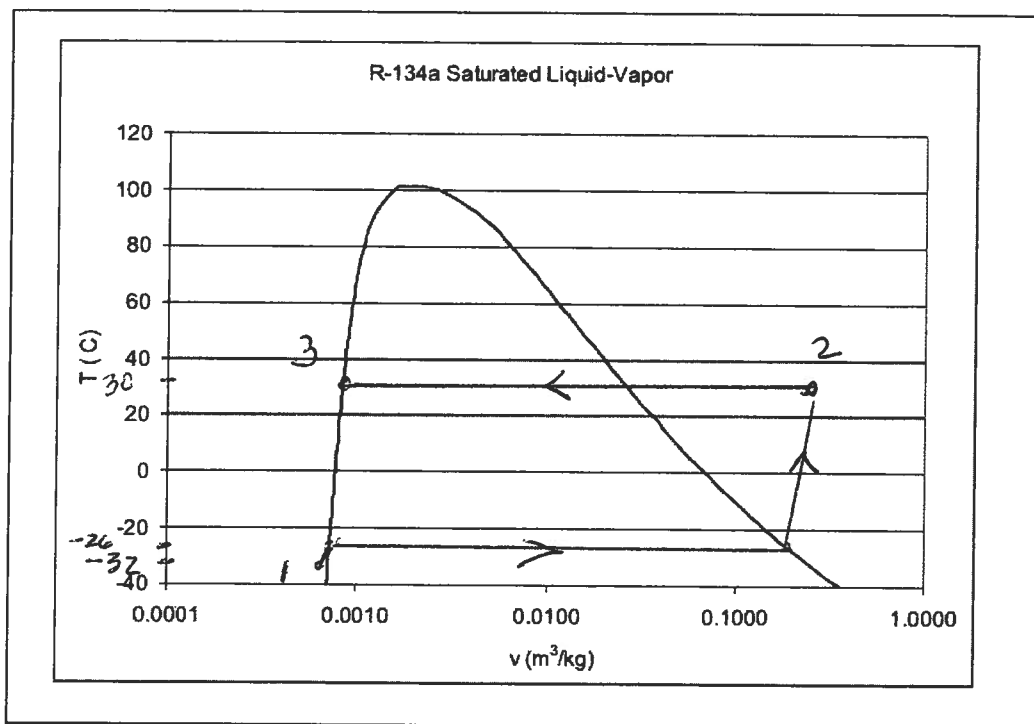
$$\Delta H = m(h_3 - h_1) = 139 \text{ kg} (93.58 - 10.1) = \boxed{11,604 \text{ kJ}}$$

11. A closed-system piston-cylinder device contains refrigerant (R-134a) at a pressure of 0.1 MPa, temperature of 241K and initial volume of 0.1 m<sup>3</sup>. The refrigerant is expanded in an isobaric process until the temperature reaches 303K.

- a) What is the mass of refrigerant in the system?
- b) What is the total volume of the system after expansion?
- c) What is the change in energy of the system during the expansion (in kJ)?

When the refrigerant temperature reaches 303K, energy is removed in an isothermal process until it is a saturated liquid.

- d) What is the pressure of the refrigerant at the end of the isothermal process?
- e) Draw the two-step process on the T-v diagram for refrigerant below using values for temperature and specific volume:



f) What is the net change in energy of the refrigerant over the two-step process?

g) Draw the two-step process on the P-v diagram for refrigerant below using values for pressure and specific volume.

